ICOZ Rec'd PCT'PTO 1 9 FEB 2002 Form PTO-1390 US DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE ATTORNEY'S DOCKET NO (Rev. 12-29-9 M 6741 HST PCT/US TRANSMITTAL LETTER TO THE UNITED STATES us APPLICATION NO 1 TO 70 0 49767 DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371 INTERNATIONAL APPLICATION NO. INTERNATIONAL FILING DATE PRIORITY DATE CLAIMED PCT/US00/22335 August 14, 2000 August 16, 1999 TITLE OF INVENTION PROCESS AND COMPOSITION FOR TREATING METALS APPLICANT(S) FOR DO/EO/US Hirokatsu Bannai, Yasuhiko Nagashima and Takaomi Nakayama Applicant herewith submits to the United States Designated/Elected Office (EO/DO/US) the following items and other information This is a FIRST submission of items concerning a filing under 35 U.S.C. 371 This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C., 371, 3 This express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U S C 371(b) and PCT Articles 22 and 39 (1) A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date A copy of the International Application as filed (35 U S.C 371(c)(2)) is transmitted herewith (required only if not transmitted by the International Bureau) h has been transmitted by the International Bureau is not required, as the application was filed in the United States Receiving Office (RO/US) ☐ A translation of the International Application into English (35 U S C 371(c)(2)) Amendments to the claims of the International Application under PCT Article 19 (35 U S C, 371(c)(3)) are transmitted herewith (required only if not transmitted by the International Bureau) b. have been transmitted by the International Bureau c ш have not been made, however, the time limit for making such amendments has NOT expired d have not been made and will not be made 8.

A translation of the amendments to the claims under PCT Article 19 (35 U S C 371(c)(3)) 9. An oath or declaration of the inventor(s) (35 U S C 371(c)(4)) 10.

A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U S C 371(c)(5)) Items 11. to 16. below concern other document(s) or information included: 11. An Information Disclosure Statement under 37 CFR 1 97 and 1 98 12. An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3 28 and 3 31 is included 13. A FIRST preliminary amendment □ A SECOND or SUBSEQUENT preliminary amendment 14. A substitute specification. 15. A change of power of attorney and/or address letter.

16. Other items or information:

International Search Report and IDC
"Express Mail" mailing label number <u>EL615775383US</u>

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PATENT

Docket No. M 6741 PCT/US

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

RF.

PCT/FP00/22335

International Filing Date: August 12, 2000
Priority Date Claimed: August 16, 1999

Applicant: Bannai et al.

Title: PROCESS FOR FORMING A PHOSPHATE CONVERSIN

COATING ON METAL Applicants' Reference: M 6741 PCT/US

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents

Box PCT

Washington, DC 20231

ATTN: DO/EO/US

Sir:

Prior to substantive examination of the above referenced application, please enter the following Amendment.

IN THE SPECIFICATION:

Page 1, after the title, enter the following new paragraph:

--This application claims priority from International Application No. PCT/US00/22335, filed 16 August 2000 and published in English, and Japanese Application No. H11-230060, filed 16 August 1999.--

Page 28, line 1, amend to read as follows:

What is claimed is:

Enter page 30 as the Abstract of the Disclosure.

IN THE CLAIMS:

Amend claim 1 to read as follows:

 (Amended) A process for forming a phosphate conversion coating on a metal substrate surface, said process comprising the following operations:

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- (I) contacting the metal substrate surface with an aqueous liquid surface conditioning composition that comprises water and the following components:
- (I.A) dispersed solid phosphate particles that:
 - (i) have a diameter no greater than 5 μm; and
 - (ii) comprise at least one substance selected from the group consisting of phosphates that contain at least one type of divalent or trivalent metal cations:

and

- (I.B) as adhesion-promoting component, at least one selection from the group consisting of the following subgroups:
 - (1) monosaccharides, polysaccharides, and derivatives thereof;
 - phosphorus containing solutes selected from the group consisting of orthophosphoric acid, condensed phosphoric acids, and organophosphonic acid compounds;
 - (3) water-soluble polymers that are homopolymers or copolymers of vinyl acetate and derivatives of these homopolymers and copolymers; and
 - (4) copolymers and polymers afforded by the polymerization of:
 - (a) at least one selection from:
 - monomers, exclusive of vinyl acetate, that conform to general chemical formula (I):

$$H_2$$
C=C-COOR² (I), where R¹ = H or CH₃ and R² = H, C₁ to C₅ alkyl, or C₁ to C₅ hydroxyalkyl; and

- other α, β-unsaturated carboxylic acid monomers; and, optionally,
- (b) not more than 50 % by weight of monomers that are not vinyl acetate and are not within the description of part (a) immediately above but are copolymerizable with said monomers that are within the description of said part (a);

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- (II) contacting the metal substrate surface as conditioned in operation (I) as described above with a nickel-free phosphate conversion treatment bath that comprises water and the following amounts of the following components:
- (II.A) from 0.5 to 5 g/l of zinc cations;

4.

- (II.B) from 5 to 30 g/l of phosphate ions; and
- (II.C) a component of conversion accelerator.Enter the following new claims 5-10:
- 5. (New) The process of claim 1 wherein the divalent or trivalent metal cations are selected from the group consisting of Zn, Fe, Mn, Co, Ca, Mg and Al.
- 6. (New) The process of claim 1 wherein the aqueous liquid surface conditioning composition has a concentration of dispersed solid phosphate particles of from 0.001 to 30 g/l.
- 7. (New) The process of claim 1 wherein the aqueous liquid surface conditioning composition has a concentration of adhesion-promoting component of from 1 to 2000 ppm.
- 8. (New) The process of claim 1 wherein the aqueous liquid surface conditioning composition is additionally comprised of an alkali metal or ammonium salt selected from the group consisting of orthophosphate salts, metaphosphate salts, orthosilicate salts, metasilicate salts, carbonate salts, bicarbonate salts, nitrate salts, nitrite salts, sulfate salts, borate salts, organic acid salts and mixtures thereof.
- 9. (New) The process of claim 1 wherein the nickel-free phosphate conversion treatment bath is additionally comprised of an etchant selected from the group consisting of fluoride ions, complex fluoride ions, and mixtures thereof.
- 10. (New) The process of claim 1 wherein the metal substrate is selected from the group consisting of steel sheets, zinc-plated steel sheets, zinc alloyplated steel sheets, magnesium alloys, and aluminum alloys.

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REMARKS

Claim 1 has been amended for clarification reasons only. The amendments to claim 1 are shown on the separate sheet entitled "Version Marked to Show Changes Made".

Respectfully submitted,

Stephen D. Harper (Reg. No. 33,243) Attorney for Applicants (610) 278-4927

Henkel Corporation Law Department 2500 Renaissance Boulevard, Suite 200 Gulph Mills, PA 19406

Version Marked to Show Changes Made

Claim 1 has been amended as follows:

- (Amended) A process for forming a phosphate conversion coating on a metal substrate surface, said process comprising the following operations:
- contacting the metal substrate surface with an aqueous liquid surface conditioning composition that comprises[, preferably consists essentially of, or more preferably consists of,] water and the following components:
- (I.A) dispersed solid phosphate particles that:
 - (i) have a diameter no greater than 5 µm; and
 - (ii) comprise at least one substance selected from the group consisting of phosphates that contain at least one type of divalent or trivalent metal cations:

and

- (I.B) as adhesion-promoting component, at least one selection from the group consisting of the following subgroups:
 - (1) monosaccharides, polysaccharides, and derivatives thereof;
 - phosphorus containing solutes selected from the group consisting of orthophosphoric acid, condensed phosphoric acids, and organophosphonic acid compounds;
 - (3) water-soluble polymers that are homopolymers or copolymers of vinyl acetate and derivatives of these homopolymers and copolymers; and
- (4) copolymers and polymers as afforded by the polymerization of:

 R^1

- (a) at least one selection from:
 - monomers, exclusive of vinyl acetate, that conform to general chemical formula (I):

$$\label{eq:H2C=COOR} I \\ H_2C=C-COOR^2 \\ \mbox{(I)}, \\ \mbox{where } R^1=H \mbox{ or } CH_3 \mbox{ and } R^2=H, \mbox{ } C_1 \mbox{ to } C_5 \mbox{ alkyl, or } C_1 \mbox{ to } C_5 \mbox{ }$$

hydroxyalkyl; and

other α, β-unsaturated carboxylic acid monomers; and,

Preliminary Amendment of U.S. National Stage for International Application PCT/US/0022335 filed August 16. 2000

optionally.

(b) not more than 50 % by weight of monomers that are not vinyl acetate and are not within the description of part (a) immediately above but are copolymerizable with said monomers that are within the description of said part (a);

and

- (II) contacting the metal substrate surface as conditioned in operation (I) as described above with a nickel-free phosphate conversion treatment bath that comprises water and the following amounts of the following components:
- (II.A) from 0.5 to 5 g/l of zinc cations;
- (II.B) from 5 to 30 g/l of phosphate ions; and
- (II.C) a component of conversion accelerator.



Description

PROCESS FOR FORMING A PHOSPHATE CONVERSION COATING ON METAL

FIELD AND BACKGROUND OF THE INVENTION

This invention relates to processes for the phosphate conversion treatment of metals wherein said processes employ a nickel ion-free phosphate conversion treatment bath and produce a uniform, strongly paint-adherent, and highly post-painting corrosion-resistant coating on such metals as steel sheet, zinc-plated steel sheet, aluminum alloys, and magnesium alloys.

Phosphate conversion treatments are currently executed as a pre-paint treatment on automotive body components in order to enhance corrosion resistance and improve the steel sheet-to-paint adherence. In these phosphate conversion treatments, the metal is first brought into contact with a colloidal titanium surface conditioning bath and is then brought into contact with an acidic solution containing phosphate ions, zinc ions, nickel ions, and manganese ions in order to precipitate a phosphate coating on the metal.

However, in association with today's heightened concern with environmental protection, the regulatory situation with regard to nickel in wastewater has become increasingly stringent, particularly in Europe. It is certainly prudent to anticipate that regulations on nickel in wastewater might also become much more demanding in other countries in the future. These considerations make it desirable to eliminate the nickel from the conversion treatment baths used in zinc phosphate treatments.

Unfortunately, a number of negative effects are caused by removal of the nickel from many phosphate treatment baths used in the aforementioned phosphate treatment processes: The crystals in the phosphate coating undergo coarsening; the phosphate coating suffers from a loss of uniformity, the post-painting corrosion resistance declines, and the secondary (water-resistant) adherence of paint to zinc-plated material also declines.

Japanese Laid Open Patent Application (PCT) Number Hei 7-505445 (505,445/1995) teaches a nickel-free phosphate treatment process in order to solve the problems referenced above. This treatment process involves formation of a nickel-free phosphate coating by treatment with a phosphate conversion bath containing 0.2 to 2 grams of zinc ions per liter of bath (this unit of concentration being freely used hereinafter for any constituent of any liquid and being usually abbreviated as "g/l"), 0.5 to 25 milligrams of copper ions per liter, and 5 to 30 g/l phosphate ions. This process

uses copper as a substitute metal for nickel, but still suffers from several problems. Since the allowable copper level in this conversion treatment bath is so very low, management of the copper concentration in real-world lines is exceedingly difficult. Another concern is with electrolytic corrosion of the equipment accompanied by displacement copper plating on parts of the equipment.

Given this background, there is a desire for development of a phosphate conversion treatment process that does not use nickel but nevertheless affords a post-painting adherence and post-painting corrosion resistance that are the equal of those afforded by existing phosphate conversion treatments that use nickel. One major object of this invention is to provide a phosphate conversion treatment process that treats metal surfaces with a nickel-free conversion treatment bath and produces a phosphate conversion coating that evidences an excellent post-painting corrosion resistance and excellent paint adherence.

BRIEF SUMMARY OF THE INVENTION

It has been found that most or all of the problems caused by the removal of nickel from previous phosphating treatments can be eliminated by using a surface conditioning composition that contains very fine, dispersed solid phosphate particles.

DETAILED DESCRIPTION OF THE INVENTION AND PREFERRED EMBODIMENTS.

More specifically, a process according to the invention for forming a phosphate conversion on a metal substrate surface comprises, preferably consists essentially of, or more preferably consists of the following operations:

- (I) contacting the metal substrate surface with an aqueous liquid surface conditioning composition (hereinafter for brevity often called a "bath" without intending any implication that it must be contacted with the metal substrate by immersion of the metal substrate in a volume of the aqueous liquid surface conditioning composition) that comprises, preferably consists essentially of, or more preferably consists of, water and the following components:
- (I.A) dispersed solid phosphate particles that:
 - have a diameter no greater than 5 micrometres, this unit of length being hereinafter usually abbreviated as "μm"; and
 - (ii) comprise, preferably consist essentially of, or more preferably consist of, at least one substance selected from the group consisting of phosphates that contain at least one divalent or trivalent metal cation; and
- (I.B) as adhesion-promoting component, at least one selection from the group

consisting of the following subgroups:

- (1) monosaccharides, polysaccharides, and derivatives thereof;
- phosphorus containing solutes selected from the group consisting of orthophosphoric acid, condensed phosphoric acids, and organophosphonic acid compounds;
- water-soluble polymers that are homopolymers or copolymers of vinyl acetate and derivatives of these homopolymers and copolymers; and
- (4) copolymers and polymers as afforded by the polymerization of:
 - (a) at least one selection from:
 - monomers, exclusive of vinyl acetate, that conform to general chemical formula (I):

$$R^1$$
 | H₂C=C-COOR² (I),

where R^1 = H or CH_3 and R^2 = H, C_1 to C_5 alkyl, or C_1 to C_5 hydroxyalkyl; and

- other α,β-unsaturated carboxylic acid monomers; and, optionally.
- (b) not more than 50 % by weight of monomers that are not vinyl acetate and are not within the description of part (a) immediately above but are copolymerizable with said monomers that are within the description of said part (a):

and

- (II) contacting the metal substrate surface as conditioned in operation (I) as described above with a nickel-free phosphate conversion treatment bath that comprises, preferably consists essentially of, or more preferably consists of water and the following amounts of the following components:
- (II.A) from 0.5 to 5 g/l of zinc cations;
- (II.B) from 5 to 30 g/l of phosphate ions; and
- (II.C) a component of conversion accelerator.

In a preferred embodiment, the above-specified conversion treatment baths also contain from 0.1 to 3.0 g/l of at least one type of metal containing ions selected from the group consisting of magnesium ions, cobalt ions, manganese ions, calcium ions, tungstate ions, and strontium ions.

The features of this invention are explained in greater detail hereinbelow.

Whenever a group of materials from which a constituent can be selected is specified, whether by a specific list, use of generic chemical terms, and/or conformance to a general chemical formula, any two or more of the group may be selected instead of a single member with equal preference, unless explicitly stated otherwise.

While no particular limitations apply to the metal on which the inventive phosphate treatment process may be executed, this metal is preferably steel sheet, zinc-plated steel sheet, zinc alloy-plated steel sheet, magnesium alloy, or aluminum alloy.

It is preferred in the practice of the invention that the metal substrate surface be clean prior to the phosphate conversion treatment. Metal whose surface is already clean can be brought without further treatment into contact with the surface conditioning bath. However, in the case of treatment of metal whose surface is contaminated with adherent materials such as iron particles, dust, and oil, the contaminants adhering on the surface should be removed by cleaning, for example, by cleaning with a water-based alkaline degreaser or an emulsion degreaser or by solvent degreasing. When a water-based cleaner is used, the cleaning bath remaining on the metal surface is preferably removed by the provision of, for example, a water rinse step after the cleaning step.

At least some of the particles of divalent and/or trivalent metal phosphate present in a surface conditioning bath in a process according to the invention must have a particle size or diameter no greater than 5 μ m. (Insolubles of larger size are undesirable because — depending on the particular circumstances — they often cannot be stably maintained in the aqueous bath.) These phosphate particles are believed to function as nuclei during phosphate crystal deposition and also to promote the deposition reaction itself, by undergoing partial dissolution in the phosphate conversion treatment bath and inducing a substantial acceleration of the initial phosphate crystal deposition reactions by supplying one or more main components of the phosphate crystals to the region immediately adjacent to the metal surface.

The divalent and trivalent metals used here are not critical, but preferably comprise at least one selection from Zn, Fe, Mn, Co, Ca, Mg, and Al. The divalent and/or trivalent metal phosphate particles are preferably present at a concentration from 0.001 to 30 g/l. Acceleration of the initial phosphate crystal deposition reactions does not normally occur at a divalent and/or trivalent metal phosphate particle concentration below 0.001 g/l due to the small amount of divalent and/or trivalent metal phosphate

particles that become adsorbed on the metal surface at such low concentrations. Concentrations below 0.001 g/l also prevent acceleration of the crystal deposition reactions due to the small number of divalent and/or trivalent metal phosphate particles available to act as crystal nuclei. Divalent and/or trivalent metal phosphate particle concentrations in excess of 30 g/l cannot be expected to provide additional promotion of the phosphate conversion reactions and hence will be uneconomical.

The adhesion-promoting component that must be present in the inventive surface conditioning bath functions to improve the dispersion stability of the divalent and/or trivalent metal phosphate particles and to accelerate adsorption of the divalent and/or trivalent metal phosphate particles onto the metal surface. More specifically, the adhesion promoting component is believed to adsorb on the surface of the divalent and/or trivalent metal phosphate particles and, through a steric hindrance activity and repulsive forces arising from its electrical charge, to prevent collisions among the divalent and/or trivalent metal phosphate particles in the surface conditioning bath and thereby inhibit their aggregation and sedimentation. In addition, due to its structure, the adhesion-promoting component itself is believed to have an ability to adsorb to metal surfaces and thereby to accelerate adsorption to metal surfaces by the divalent and/or trivalent metal phosphate particles, so that the surface conditioning activity manifests upon contact between the metal workpiece and surface conditioning bath.

The adhesion-promoting component concentration is preferably from 1 to 2,000 parts by weight of the adhesion promoting component per 1000 parts by weight of the total conditioning composition, this unit of concentration being hereinafter usually abbreviated as "ppm". At concentrations below 1 ppm a surface conditioning activity can not usually be produced just by contact between the metal workpiece and the surface conditioning bath. Not only can no additional benefit be expected at concentrations in excess of 2,000 ppm, but such concentrations can impair the phosphate conversion coating formed, perhaps as a result of excessive adsorption of the adhesion promoting component on the metal substrate surface.

A saccharide type of adhesion-promoting component for the surface conditioning operation in a process according to the invention may be exemplified by fructose, tagatose, psicose, sorbose, erythrose, threose, ribose, arabinose, xylose, lyxose, allose, altrose, glucose, mannose, gulose, idose, galactose, talose, and the sodium and ammonium salts of all of these saccharides.

A phosphorus containing acid type of adhesion-promoting component in the sur-

face conditioning process is exemplified by orthophosphoric acid, polyphosphoric acids, and organophosphonic acid compounds, or more individually by pyrophosphoric acid, triphosphoric acid, trimetaphosphoric acid, tetrametaphosphoric acid, hexametaphosphoric acid, aminotrimethylenephosphonic acid, 1-hydroxyethylidene-1,1-diphosphonic acid, ethylenediaminetetramethylenephosphonic acid, diethylenetriaminepentamethylenephosphonic acid, and the sodium and ammonium salts of all of the preceding acids. Sodium salts are preferred for the organophosphonic acids if they are to be used in salt form.

Polymeric adhesion promoting components derived from polyvinylacetate in a surface conditioning operation in a process according to the invention are exemplified by polyvinyl alcohols afforded by the hydrolysis of vinyl acetate polymers, cyanoethylated polyvinyl alcohols afforded by the cyanoethylation of polyvinyl alcohol with acrylonitrile, formalated polyvinyl alcohols afforded by the acetalation of polyvinyl alcohol with formaldehyde, urethanized polyvinyl alcohols afforded by the urethanation of polyvinyl alcohol with urea, and water-soluble polymers afforded by the introduction of carboxyl moieties, sulfonic moieties, or amide moieties into polyvinyl alcohol. Suitable vinyl acetate-copolymerizable monomers are exemplified by acrylic acid, crotonic acid, and maleic anhydride. The effects associated with the present invention will be fully manifested as long as the vinyl acetate polymer or derivative thereof or the copolymer of vinyl acetate and vinyl acetate-copolymerizable monomer is soluble in water. Within this limitation, these effects are independent of the degree of polymerization and the degree of functional group introduction of the subject polymers.

Suitable monomers for other polymeric adhesion promoting components for the surface conditioning operation are exemplified by: methyl acrylate, ethyl acrylate, propyl acrylate, butyl acrylate, pentyl acrylate, hydroxymethyl acrylate, hydroxyethyl acrylate, hydroxypentyl acrylate, hydroxypentyl acrylate, hydroxymethyl methacrylate, hydroxybethyl methacrylate, hydroxypentyl methacrylate, hydroxybethyl methacrylate, and hydroxypentyl methacrylate as examples of polymers according to formula (I); acrylic acid, methacrylic acid, and maleic acid as unsaturated acids; and styrene, vinyl chloride, and vinylsulfonic acid as optional comonomers.

A surface conditioning bath used by the inventive phosphate treatment processes can also optionally contain an alkali metal salt or ammonium salt or a mixture thereof, selected from the group consisting of orthophosphate salts, metaphosphate salts, orthosilicate salts, metasilicate salts, carbonate salts, bicarbonate salts, nitrate

salts, nitrite salts, sulfate salts, borate salts, organic acid salts, and combinations of two or more selections from the aforesaid alkali metal and ammonium salts. The concentration of this component is not critical, but when used is preferably from 0.5 to 20 g/l. The surface conditioning bath may also contain a surfactant to promote uniform wetting of the surface being treated.

The phosphate conversion treatment process of this invention will now be considered in greater detail. A zinc ions concentration below 0.5 g/l, because it can prevent the formation of a coating of acceptable weight and can result in a diminished coverage ratio by the deposited phosphate crystals, can produce an inadequate post-painting corrosion resistance. A zinc ions concentration in excess of 5.0 g/l can cause a coarsening of the coating crystals, resulting in particular in a decline in the post-painting adherence. The use of a phosphate ions concentration below 5.0 g/l strongly impairs the production of a normal conversion coating. Concentrations in excess of 30.0 g/l are uneconomical since they provide no additional effect. Phosphate ions can be supplied by the addition of phosphoric acid or its aqueous solution to the phosphate conversion treatment bath or by the dissolution of, for example, sodium, magnesium, or zinc phosphate in the phosphate conversion treatment bath.

The conversion treatment bath also contains a component known as a "conversion accelerator" or simply "accelerator". The accelerator acts to restrain gaseous hydrogen production during etching, an action sometimes called "depolarizing" the metal substrate surface. Otherwise, however, no particular limitations apply to the accelerator, and any material or combination of materials recognized as a conversion accelerator in prior art may be used.

The phosphate conversion treatment bath of this invention can also contain from 0.1 to 3.0 g/l of at least one type of metal containing ions selected from the group consisting of magnesium cations, cobalt cations, manganese cations, calcium cations, tungstate anions, and strontium cations. The presence of this component in the phosphate conversion treatment bath, through its incorporation into the phosphate coating and through its precipitation in a form separate from the phosphate, provides additional performance enhancements in the post-painting corrosion resistance and post-painting adherence, respectively. The use of a concentration below 0.1 g/l usually does not effect any improvement in painting performance. A concentration above 3.0 g/l is economically wasteful, since no additional improvements in painting performance usually results; a high concentration can actually hinder deposition of the zinc phosphate that

is the main component of an effectively protective conversion coating produced according to this invention. The source of one of the types of metal cations can be, for example, an oxide, hydroxide, carbonate, sulfate, nitrate, or phosphate of the particular metal. The source of tungstate can be, for example, the sodium or potassium salt.

An etchant may be added to the phosphate conversion treatment bath in order to induce a uniform etch of the surface of the metal workpiece. Usable as this etchant are, for example, fluoride ions and complex fluoride ions such as fluorosilicate ions. The fluorine compound used here can be, for example, hydrofluoric acid, fluorosilicic acid, or a water soluble metal salt (e.g., sodium salt, potassium salt) of the preceding.

The phosphate conversion treatment can be carried out by immersion or spraying or some combination thereof. Treatment for about 1 to 5 minutes can form a conversion coating satisfactorily robust for practical applications. The temperature of the phosphate conversion treatment bath is preferably from 30 to 60 °C.

The phosphate conversion treatment is preferably followed by at least one water rinse, and deionized water is preferably used in the final water rinse.

Working and comparative examples of actual treatments are provided below in order to demonstrate the advantageous effects of this invention in specific terms. The working examples that follow are simply examples of the application of the invention and in no way limit the applications of the invention or materials usable in the application of the invention.

Materials tested

The following metal substrates were treated in the working and comparative examples: electrogalvanized steel sheet ("EG"), sheet thickness = 0.8 millimeters (here-inafter usually abbreviated as "mm"), plating add-on = 20 grams of plated zinc per square meter of sheet surface, this unit of coating weight being hereinafter freely used for any coating on any surface and being hereinafter usually abbreviated as "g/m²; galvannealed hot-dip galvanized steel sheet ("GA"), sheet thickness = 0.8 mm, coating add-on = 45 g/m²; and cold-rolled steel sheet ("CRS"), sheet thickness = 0.8 mm, type SPCC-SD

Treatment operations sequence (common to the working and comparative examples; as noted in the description of the testing below, not all of the specimens tested were subjected to the operations numbered 8 or higher)

 Degreasing with diluted FINECLEANER® L4460 alkaline degreaser concentrate, a product of Nihon Parkerizing Co., Ltd., the working degreaser containing 20 g/I of agent A and 12 g/I of agent B, 43 °C, 120 seconds, dipping.

- (2) Water rinse with tapwater: ambient temperature, 30 seconds, spray.
- (3) Surface conditioning

The conditions are described below in the tables for the working and comparative examples. The colloidal titanium surface conditioning treatments were run using PREPALENE® ZN, a product of Nihon Parkerizing Co., Ltd.

(4) Phosphate conversion treatment

The conditions are described below in the tables for the working and comparative examples. The treatment time was 120 seconds in all cases.

- (5) Water rinse (tapwater): ambient temperature, 30 seconds, spray
- (6) Deionized water rinse (deionized water with an electrical conductivity ≤ 0.2 microSiemens per centimeter): ambient temperature, 20 seconds, spray
- (7) Drain/dry: 120 seconds, forced hot air at 90 °C
- (8) Cationic electrocoating to a film thickness of about 20 μm, then bake for 20 minutes at 180 °C
- (9) Surface coating with a film thickness of about 40 μm baked for 20 minutes at 140
 °C
- (10) Top coating with a film thickness of about 40 μm baked for 20 minutes at 140 $^{\circ}\text{C}.$

Test and other evaluation methods

The coating appearance was evaluated on the following two-level scale (after operation (7) as described above:

+ : the coating was uniform;

the coating exhibited a significant lack of uniformity with visible voids.

The test conditions and evaluation scale for the secondary (water-resistant) adherence were as follows: The sheet after operation (10) as described above was immersed for 240 hours in a hot water bath (maintained at 40 °C) that was being bubbled with air. The sheet was allowed to stand for 2 hours after removal from the hot water bath, after which time the peeling behavior was evaluated by cutting a grid (2 mm on each edge) in the sheet and subjecting this to tape peeling. The peeling behavior was evaluated using the following three-level scale:

++ : complete absence of peeling:

some peeling observed at the edges of the grid cut;

substantial peeling.

The test conditions and evaluation scale for the hot saltwater immersion test

were as follows. A cross cut was scribed with an acrylic cutter in the sheet after operation (8) as described above, and the specimen thus prepared was immersed for 240 hours in a 5 % by weight solution of sodium chloride in water that was maintained at 55 °C and was bubbled with air. The specimen was allowed to stand for 1 hour after withdrawal from the saltwater bath, after which time the cross cut was peeled with tape and the width of peeling from the cut was evaluated. The peeling behavior was evaluated using the following three-level scale:

For the CRS:

+ + : maximum peel width (both sides) less than 4 mm;

maximum peel width (both sides) at least 4 mm but less than 6 mm;

x : maximum peel width (both sides) at least 6 mm.

For the EG and GA:

+ + : maximum peel width (one side) less than 3 mm;

+ : maximum peel width (one side) at least 3 mm but less than 5 mm:

x : maximum peel width (one side) at least 5 mm.

The test conditions and evaluation scale for salt spray testing were as follows: A cross cut was scribed with an acrylic cutter in the sheet after operation (8) as described above, and the specimen thus prepared was tested using a salt spray tester (5 % by weight solution of sodium chloride in water) maintained at 35 °C. After the stipulated time (based on Japanese Industrial Standard Z-2371), the specimen was rinsed with water and the status of corrosion at the cross cut was evaluated using the following three-level scale:

For the CRS (salt spray test time = 960 hours):

+ + : maximum rust width (both sides) less than 4 mm:

+ : maximum rust width (both sides) at least 4 mm but less than 5 mm;

× : maximum rust width (both sides) at least 5 mm.

For the EG and GA (salt spray test time = 480 hours):

+ + : maximum rust width (one side) less than 4 mm:

+ : maximum rust width (one side) at least 4 mm but less than 5 mm;

x : maximum rust width (one side) at least 5 mm.

Details of the surface conditioning processes and phosphate treatment processes for the Examples and Comparative Examples and the corresponding test results are reported in the following tables, in which the following abbreviations are used:

Process Conditions:

for the phosphate salt component:

7n2FeP2 Zn₂Fe(PO₄)₂•4H₂O

Zn3P2 Zn₃(PO₄)₂•4H₂O

Zn2CaP2 Zn₂Ca(PO₄)₂•4H₂O

for the surfactant component:

EO11NPE polyoxyethylene (EO: 11) nonylphenol ether

for the phosphorus compounds:

Polym. =

PVAIc

ATMPA = aminotrimethylenephosphonic acid

1-HEDPA 1-hydroxyethylidene-1,1-diphosphonic acid

2-HEDPA 2-hydroxyethylidene-1.1-diphosphonic acid

polyvinylalcohol

EDATMPA ethylenediaminetetramethylenephosphonic acid.

other:

Dea. Degree

Ex. Example

Polymerization Comp. Ex. Comparative Example

VA vinyl acetate

Wt% Percent by weight.

Table 1: EXAMPLES 1 TO 5

				Exan	iple Numbe	r:	
			1	2	3	4	5
	PREP.	ALENE®-ZN, g/l	none	none	none	none	none
	D1	Abbreviation	Zn2FeP2	Zn2FeP2	Zn2FeP2	Zn2FeP2	Zn2FeP2
	Phosphate Particles:	Particle size, µm	0.5	0.5	. 0.5	0.5	0.5
	I III ticicsi	Concentration, g/l	1	1	1	1	1
		Monosaccharide Unit	glucose	glucose	glucose	glucose	fructose
urface Condi-	Sacchar- ide-Based	Substituent(s)	CH ₂ COO H	CH ₂ COO	CH ₂ COO H	none	none
ioning Treat-	Constitu- ents:	Deg. of Substitution	NO ₂ ≤ 1.8	NO ₂ ≤ 1.8	0.7	none	0
ment		Deg. of Polym.	≤ 3,000	≤ 3,000	≤ 100	1	≤ 100
Com-		Concentration, ppm	5	1,000	10	2,000	2,000
posi- tion	Salt con- stituent(s)	Chemical Formula	none	none	NaNO ₂	MgSO ₄ • 7H ₂ O	none
Con- stitu-	:	Concentration, g/l	none	none	0.5	0.5	none
ents and				11			

	-	411					
	Sur- factant	Abbreviation	none	none	none	none	none
	Constit- uents:	Concentration, g/l	none	none	none	none	none
		nt Temperature, °C	20	20	20	20	20
	Treatm	ent Time, Seconds	30	30	30	30	30
		PO4 ³ -	10	15	20	18	16
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4
		Mg ²⁺	2.0	none	none	none	2.5
Phos-		Co2+	none	1.0	none	none	none
phate		Mn ²⁺	0.5	none	1.0	none	none
Con-	C	Ca ²⁺	none	none	none	1.5	none
version Treat-	Grams per Liter of:	Sr ²⁺	none	none	none	none	0.9
ment	of:	WO ₄ -2	none	none	0.3	none	none
Com-		NO ₃ -	8.3	7.6	9.0	8.0	7.3
posi- tion		F-	0.1	none	0.1	none	0.1
Con-		NO ₂ -	0.01	none	0.01	none	0.01
stitu-		NH ₄ OH	none	1.5	none	3.0	none
ents and	Treatmen	nt Temperature, °C	40	45	50	35	43
Process	Treatm	ent Time, Seconds	120	120	120	120	120
Condi- tions:							

Table 2: EXAMPLES 6 TO 10

				Ex	ample Num	ber:	7
			6	7	8	9	10
	PREPA	ALENE®-ZN, g/l	none	none	none	none	none
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2CaP2
	Phosphate	Particle size, µm	0.5	0.6	1.2	0.4	0.4
	Particles:	Concentration, g/l	1	1	1	10	5
		Monosaccharide Unit	glucose	glucose	glucose	glucose	fructose
			xylose	ĺ			
Surface	Sacchar-		galactose				
Condi-	ide-Based	Substituent(s)	none	CH2COOH	CH ₂ COOH	CH ₂ COOH	none
tioning	Constitu- ents:	~			CH ₃		
Treat-	ents:	Deg. of Substitution	0	≥ 2	1.9	1.0	0
ment		Deg. of Polym.	≤ 500	≤ 200	≤ 1,000	≤ 2,000	≤ 500
Com-		Concentration, ppm	100	100	1	10	5
position	Salt con-	Chemical Formula	none	none	Na ₂ O•SiO	Na ₂ CO ₃	Na ₃ PO ₄ •
	stituent(s):	Concentration, g/l			2•5H ₂ O	1	12H ₂ O
uents	Surfactant	Abbreviation	none	none	none		EO11NPE
and	Constit-	Concentration, g/l	none	none		none	2.0
Process Condi-	uents:	Concentration, g/i	none	none	none	none	2.0
tions:		t Temperature, °C	20	20	20	20	40
uons.		ent Time, Seconds	30	30	30	30	120
	21000	PO ₄ 3-	11	15	22	18	16
		Zn ²⁺	0.9	1.3	2.0	1.5	1.4
		Mg ²⁺	2.0	none	none	none	2.5
Phos-		Co ²⁺	none	none	none	none	none
phate		Mn ²⁺	0.6	none	1.0	none	none
Conver-		Ca ²⁺	none	none	none	1.0	none
sion		Sr ²⁺	none	none	none	none	0.9
Treat- ment	Grams per Liter	WO ₄ -2	none	none	0.3	none	none
Compo-	of:	NO ₃ -	8.9	7.6	9.0	8.0	7.3
sition	01.	F-	0.1	none	0.1	none	0.1
Constit-		NO ₂ -	0.01	none	0.01	none	none
uents		NH ₄ OH	none	1.5	none	3.0	3.5
and	Treatmen	t Temperature, °C	38	43	49	55	59
Process	Treatme	ent Time, Seconds	120	120	120	120	120
Condi-							
tions:							

Table 3: COMPARATIVE EXAMPLES 1 TO 5

Γ				Comparativ	e Example l	Number:	
			1	2	3	4	5
	PREP.	ALENE®-ZN, g/I	none	none	none	none	none
l		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn3P2	Zn3P2
	Phosphate	Particle size, µm	0.5	0.6	1.2	-0.5	0.5
	Particles:	Concentration, g/l	1	1	1	1	1
	Sacchar-	Monosaccharide Unit	glucose xylose galactose	glucose	glucose	glucose	fructose
Surface Condi-	ide-Based Constitu-	Substituent(s)	none	-	СН ₂ СООН СН3	none	none
tioning Treat-	ents:	Deg. of Substitution	0	≥ 2	1.9	none	none
ment		Deg. of Polym.	≤ 500	≤ 200	≤ 1,000	1	≤ 100
Com-		Concentration, ppm	100	100	1	2000	2000
position Constit-	Salt con- stituent(s):	Chemical Formula	none	none	Na ₂ O•SiO ₂ •5H ₂ O	MgSO ₄ • 7H ₂ O	none
uents	` ' '	Concentration, g/l	none	none	5	0.5	none
and	Surfactant	Abbreviation	none	none	none	none	none
Process Condi-	Constit- uents:	Concentration, g/l	none	none	none	none	none
tions:	Treatmen	nt Temperature, °C	20	20	20	20	20
	Treatme	ent Time, Seconds	30_	30	30	30	30
		PO ₄ 3-	11	15	1.0	18	16
		Zn ²⁺	0.1	7.0	2.0	1.5	1.4
Phos-		Mg ²⁺	2.0	none	none	none	2.5
phate		Co ²⁺	none	none	none	none	none
Conver-		Mn ²⁺	0.6	none	1.0	1.0	none
sion		Ca ²⁺	none	none	none	none	none
Treat-	i	Sr ²⁺	none	none	none	3.0	0.9
ment Compo-	ļ	WO ₄ -2	none	none	0.3	none	none
sition	Grams	NO ₃ -	8.9	7.6	9.0	8.0	7.3
Constit-	per Liter	F-	0.1	none	0.1	none	0.1
uents	of:	NO ₂ -	0.01	none	0.01	none	none
and		NH4OH	none	1.5	none	3.0	3.5
Process Condi-		ıt Temperature, °C	38	43	49	55	20
tions:	Treatme	ent Time, Seconds	120	120	120	120	120

Table 4: COMPARATIVE EXAMPLES 6 TO 10

				Compa	rative Exan	iple Number	r:
			6	7	8	9	10
	PREP	ALENE®-ZN, g/l	1	none	none	none	none
		Abbreviation	none	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
	Phosphate	Particle size, µm	none	0.6	6.5	0.4	0.5
	Particles:	Concentration, g/l	none	1	_1	10	0.00001
		Monosaccharide Unit	none	none	glucose	glucose	glucose
	a 1	Substituent(s)	none	none	CH ₂ COOH	CH ₂ COOH	CH ₂ COOH
Surface	Sacchar- ide-Based				CH ₃		
Condi-	Constitu-	Deg. of Substitution	none	none	1.9	1.0	0.7
tioning	ents:	Deg. of Polym.	none	none	≤ 1,000	≤ 2,000	≤ 100
Treat-		Concentration, ppm	none	none	1	5,000	10
ment	Salt con-	Chemical Formula	none	none	Na ₂ O•SiO	Na ₂ CO ₃	NaNO ₂
Com-	stituent(s):				2 • 5H2O		
position		Concentration, g/l	none	none	5	1	0.5
	Surfactant	Abbreviation	none	none	none	none	none
uents	Constit- uents:	Concentration, g/l	none	none	none	none	none
and		ıt Temperature, °C	20	20	20	20	20
Process Condi-		ent Time, Seconds	30	30	30	30	30
tions:	Treatm	ent Time, Seconds	30	30	30	30	30
tions.		PO ₄ 3-	11	15	22	18	16
		Zn ²⁺	0.9	1.3	2.0	1.5	1.4
		Mg2+	2.0	none	none	none	2.5
Phos-		Co2+	none	none	none	none	none
phate		Mn ²⁺	0.6	none	1.0	none	none
Conver-		Ca ²⁺	none	none	none	1.0	none
sion		Sr ²⁺	none	none	none	none	0.9
Treat-		WO₄-2	none	none	0.3	none	none
Compo-	i	NO ₃ -	8.9	7.6	9.0	8.0	7.3
sition	Grams	F-	0.1	none	0.1	none	0.1
Constit-	per Liter	NO ₂ -	0.01	none	0.01	none	none
uents	of:	NH ₄ OH	none	1.5	none	3.0	3.5
and	Treatmer	ıt Temperature, °C	40	45	50	39	43
Process		ent Time, Seconds	120	120	120	120	120
Condi-		·			1		
tions:					L		

Table 5: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR EXAMPLES 1 THROUGH 10

TEST OR OTHER RATING	SUB-			Е	XAMP	LE N	UMBI	ER			
	STRATE TESTE D	1	2	3	4	5	6	7	8	9	10
Coating Appearance	CRS	+	+	+	+	+	+	+	+	+	+
	EG	+	+	+	+	+	+	+	+	+	+
	GA	+	+	+	+	+	+	+	+	+	+
Secondary (Water-Resistant)	CRS	++	++	++	++	++	+	++	++	++	++
Adherence	EG	++	++	+	++	++	++	++	+	++	++
	GA	++	++	+	++	++	+	++	+	++	++
	CRS	++	++	++	++	+	++	+	++	++	+
Resistance to Hot Salt Water	EG	++	++	++	++	++	++	+	++	++	++
	GA	++	++	++	++	++	++	+	++	++	++
	CRS	+	++	++	+	+	+	+	+	++	+
Resistance to Salt Spray	EG	++	+	++	+	++	++	+	+	++	++
	GA	++	+	++	+	++	++	+	+	++	++

Table 6: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR COMPARISON EXAMPLES 1 THROUGH 10

TEST OR OTHER RATING	SUB-	STRATE 1 2 3 4 5 6 7 8 9									
	STRATE TESTE D	1	2	3	4	5	6	7	8	9	10
	CRS	×	+	×	×	×	+	×	×	×	×
Coating Appearance	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	+	+	++	++	++	+	++	++	++	+
Secondary (Water-Resistant)	EG	×	×	×	×	×	×	×	×	×	×
Adherence	GA	×	×	×	×	×	×	×	×	×	×
	CRS	×	++	×	×	×	++	×	×	×	×
Resistance to Hot Salt Water	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	×	×	×	×	×	×	×	×	×	×
Resistance to Salt Spray	EG	×	+	×	×	×	+	×	×	×	×
	GA	×	×	×	×	×	×	×	×	×	×

Table 7: Examples 11 to 15

			Example Number: 11 12 13 14 15									
			11	12	13	14	15					
	PREPA	ALENE®-ZN, g/l	none	none	none	none	none					
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2					
	Phosphate	Particle size, µm	0.5	0.5	1.7	0.6	0.5					
	Particles:	Concentration, g/l	5	1	1	5	10					
	Phosphor-	Substance	tripoly-	hexameta-	ATMPA	1-HEDPA	EDATMPA					
	us Con-		phos-	phosphoric			!					
Surface	taining		phoric	acid			!					
Condi-	Solute:		acid									
tioning		Concentration, ppm	1	100	500	50	1,000					
Treat-	Salt con-	Chemical Formula	MgSO4• 7H2O	Na ₂ O • SiO 2 • 5H ₂ O	none	Na ₂ CO ₃	Na ₃ PO ₄ •1 2H ₂ O					
	stituent(s):	Concentration, g/l	0.5	1	none	5	10					
Com-	Surfactant	Abbreviation	none	none	none	none	EO11NPE					
position	Constit-	Concentration, g/l	none	none	none	none	2.0					
Constit-	uents:	Concentration, gri	none	none	none	lione	2.0					
uents and	Treatmen	t Temperature, °C	20	20	20	20	40					
Process	Treatme	ent Time, Seconds	30	30	30	30	120					
Condi-												
tions:												
		PO ₄ 3-	10	15	20	18	16					
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4					
		Mg ²⁺	2.0	none	none	none	2.5					
Phos-		Co ²⁺	none	1.0	none	none	none					
phate		Mn ²⁺	0.5	none	1.0	none	none					
Conver- sion		Ca ²⁺	none	none	none	1.5	none					
Treat-		Sr ²⁺	none	none	none	none	0.9					
ment		WO_4^{-2}	none	none	0.3	none	none					
Compo-		NO ₃ -	8.3	7.6	9.0	8.0	7.3					
sition	Grams	F-	0.1	none	0.1	none	0.1					
Constit-	per Liter	NO ₂ -	0.01	none	0.01	none	0.01					
uents	of:	NH ₄ OH	none	1.5	none	3.0	none					
and	Treatmen	t Temperature, °C	40	45	50	39	43					
Process	Treatme	ent Time, Seconds	120	120	120	120	120					
Condi-												
tions:												

Table 8: COMPARATIVE EXAMPLES 11 TO 15

	PREPALENE®-ZN, g/l none none						
			11	12	13	14	15
	PREPA	LENE®-ZN, g/l	none	none	none	none	none
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
1		Particle size, µm	0.5	0.5	1.7	0.6	0.5
	Particles:	Concentration, g/l	5	1	1	5	10
l		Substance	tripoly-		ATMPA		EDATMPA
						HEDPA	
Surface				acid			İ
	Solute:			100			
			1	100	500	50	1,000
			MgSO4	NaOH		No-CO-	Na-PO 1
Com-		Chemical Formula	•7H2O	Haon	none	Na ₂ CO ₃	2H ₂ O
position	stituent(s):	Concentration, g/l	0.5	1	none	5	10
Constit- uents	Surfactant	Abbreviation	none	none	none	none	EO11NPE
and	Constit-	Concentration, g/l	none	none	none	none	2.0
Process	uents:	, ,					
Condi-		t Temperature, °C	20	20	20	20	40
tions:	Treatme	nt Time, Seconds	30	30	30	30	120
		PO ₄ 3-	11	15	1.0	18	16
		Zn ²⁺	0.1	7.0	2.0	1.5	1.4
Phos-		Mg ²⁺	2.0	none	none	none	2.5
phate		Co ²⁺	none	none	none	none	none
Conver-		Mn ²⁺	0.6	none	1.0	1.0	none
sion		Ca ²⁺	none	none	none	none	none
Treat-		Sr ²⁺	none	none	none	3.0	0.9
ment Compo-		WO ₄ -2	none	none	0.3	none	none
sition	Grams	NO ₃ -	8.9	7.6	9.0	8.0	7.3
Constit-	per Liter	F-	0.1	none	0.1	none	0.1
uents	of:	NO ₂ -	0.01	none	0.01	none	none
and		NH ₄ OH	none	1.5	none	3.0	3.5
Process Condi-		t Temperature, °C	40	45	50	39	20
tions:	Treatme	nt Time, Seconds	120	120	120	120	120

Table 9: COMPARATIVE EXAMPLES 16 TO 20

			T	Comp	arative F	xample Numbe	r:
			16	17	18	19	20
	PREP	ALENE®-ZN, g/I	1	none	none	none	none
		Abbreviation	none	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
	Phosphate	Particle size, µm	none	0.5	6.5	0.6	0.00001
	Particles	Concentration, g/l	none	1	1	5	10
	Phosphor-	Substance	none	none	ATMPA	hexametaphos-	EDATMPA
	us Con-					phoric acid	
Surface	taining Solute	Concentration, ppm	none	none	500	3,000	1,000
Condi- tioning	Salt con-	Chemical Formula	MgSO ₄	none	none	Na ₂ CO ₃	Na ₂ O•SiO ₂
Treat-	stituent(s)		711				•5H ₂ O
ment			7H ₂ O				
Com-			0.5	none	none	5	FOLUMBE
position	Surtactant Constit-		none	none	none	none	EOLINPE
Constit-	uents	Concentration, g/l	none	none	none	none	2.0
uents and	Treatmen	nt Temperature, °C	20	20	20	20	40
Process		ent Time, Seconds	30	30	30	30	120
Condi-							
tions:						- 10	
		PO ₄ 3- Zn ²⁺	11	15	22	18	16
Phos-		Mg ²⁺	0.9	1.3	2.0	1.5	1.4
phate		Co2+	2.0	none	none	none	2.5
Conver-		Mn2+	none	none	none	none	none
sion		Ca ²⁺	0.6	none	1.0	none	none
Treat-		Sr ²⁺	none	none	none	1.0	none
ment	Grams	WO ₄ -2	none	none	none	none	0.9
Compo-	per Liter		none	none	0.3	none	none
sition	of:	NO ₃ -	8.9	7.6	9.0	8.0	7.3
Constit-		NO2-	0.1	none	0.1	none	0.1
uents				none	0.01	none	none
and	Tuestri	NH ₄ OH	none	1.5	none	3.0	3.5
Process		nt Temperature, °C	40	45	50	39	43
Condi- tions:	1 reatm	ent Time, Seconds	120	120	120	120	120
tions:							

Table 10: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR EXAMPLES 11 THROUGH 15

TEST OR OTHER RATING	SUBSTRATE	Example Number							
	TESTED	11	12	13	14	15			
Coating Appearance	CRS	+	+	+	+	+			
	EG	+	+	+	+	+			
	GA	+	+	+	+	+			
	CRS	++	++	++	++	++			
Secondary (Water-Resistant)	EG	++	++	+	++	++			
Adherence	GA	++	++	+	++	++			
	CRS	++	++	++	++	+			
Resistance to Hot Salt Water	EG	++	++	++	++	++			
	GA	++	++	++	++	++			
	CRS	+	++	++	+	+			
Resistance to Salt Spray	EG	++	+	++	+	++			
	GA	++	+	++	+	++			

Table 11: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR COMPARISON EXAMPLES 11 THROUGH 20

TEST OR OTHER RATING	SUB-		C	OMPAR	uson i	Exan	1PLE	NUM	IBER		
	STRATE TESTE D	11	12	13	14	15	16	17	18	19	20
	CRS	×	+	×	×	×	+	×	×	×	×
Coating Appearance	_EG_	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	++	+	++	++	++	+	++	++	++	+
Secondary (Water-Resistant)	EG	×	×	×	×	×	×	×	×	×	×
Adherence	GA	×	×	×	×	×	×	×	×	×	×
	CRS	×	++	×	×	×	++	×	×	×	×
Resistance to Hot Salt Water	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	×	×	×	×	×	×	×	×	×	×
Resistance to Salt Spray	EG	×	+	×	×	×	+	×	×	×	×
	GA	×	×	×	×	×	×	×	×	×	×

Table 12: EXAMPLES 16 TO 20

			I	Ex	ample Num	ber:	
			16	17	18	19	20
	PREP	ALENE®-ZN, g/l	none	none	none	none	none
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
	Phosphate	Particle size, µm	0.5	1.5	0.5	1.6	0.3
	Particles	Concentration, g/l	5	8	1	5	10
	Water	Substance Name	polyvinyl	carboxyl-	sulfonic	Copolymer	Copolyme
	Soluble		alcohol	modified	acid-	with VA	r with VA
Surface	VA			PVAlc	modified		
Condi-	Polymer				PVAlc		
tioning	or	Comonomer with	none	none	none	maleic acid	crotonic
Treat-	Derivative	VA					acid
ment		Comonomer % by	none	none	none	80	70
Com-		Weight					
position		Concentration, ppm	11	500	2,000	1,000	10
Constit-	Salt con-	Chemical Formula	MgSO ₄	Na ₂ O•SiO	none	Na ₂ CO ₃	Na ₃ PO ₄
uents	stituent(s)		•7H2O	•5H ₂ O			•12H ₂ O
and		C	0.5	•5H ₂ O			
Process	Surfactant	Concentration, g/l	0.5	. 1	none	5	10
Condi-	Constit-		none	none	none	none	EO11NPE
tions:	uents	Concentration, g/l	none	none	none	none	2.0
		t Temperature, °C	20	20	20	20	40
		ent Time, Seconds	30	30	30	30	120
	Treatme	PO ₄ 3-	10	15	20	18	16
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4
		Mg ²⁺	2.0	none	none	none	2.5
Phos-		Co2+	none	1.0			
phate		Mn ²⁺	0.5	none	none 1.0	none	none
Conver-		Ca ²⁺	none	none	none	1.5	
sion		Sr ²⁺	none	none	none	none	none 0.9
Treat-	Grams	WO ₄ -2	none	none	0.3		
ment	per Liter	NO ₃ -	8.3	7.6	9.0	none 8,0	7.3
Compo-	of:	F-	0.1	none	0.1	none	0.1
sition		NO ₂ -	0.01	none	0.01	none	0.01
Constit-		NH ₄ OH	none	1.5	none	3.0	none
uents and	Treatmen	t Temperature, °C	40	45	50	39	43
Process		ent Time, Seconds	120	120	120	120	120
Condi-	Treatme	, becomes	120	120	120	120	120
tions:							
******		`					

Table 13: COMPARATIVE EXAMPLES 21 TO 25

		***		Comparative	Example N	Number:	
			21	22	23	24	25
	PREPA	LENE®-ZN, g/l	none	none	none	none	none
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn3P2
	Phosphate	Particle size, µm	0.5	0.5	0.5	1.6	0.5
	Particles:	Concentration, g/l	5	1	1	5	1
	Water	Substance Name	polyvinyl-	carboxyl-	sulfonic	Copoly-	Copoly-
	Soluble VA		alcohol	modified	acid-modi-	mer with	mer with
Surface	Polymer	0 11		PVAlc	fied PVAlc	VA	VA
Condi-	or	Comonomer with VA	none	none	none	maleic acid	crotonic acid
tioning	Derivative	Comonomer % by	none	none	none	80	70
Treat-	:	Weight	Hone	none	Hone	80	/0
ment Com-		Concentration,	1	500	2,000	1,000	10
position		ppm			_,	1,200	
Constit-	Salt con-	Chemical	MgSO ₄ •	Na ₂ O•SiO ₂	none	Na ₂ CO ₃	Na ₃ PO ₄
	stituent(s):	Formula	7H ₂ O	•5H ₂ O			•12H2Ō
and		Concentration, g/l	0.5	1	none	5	10
Process	Surfactant Constit-		none	none	none	none	EO11NPE
Condi-	uents:	Concentration, g/l	none	none	none	none	2.0
tions:	Treatment	Temperature, °C	20	20	20	20	40
	Treatmen	nt Time, Seconds	· 30	30	30	30	120
		PO ₄ 3-	11	15	1.0	18	16
		Zn ²⁺	0.1	7.0	2.0	1.5	1.4
Phos-		Mg ²⁺	2.0	none	none	none	2.5
phate		Co ²⁺	none	none	none	none	none
Conver-		Mn ²⁺	0.6	none	1.0	1.0	none
sion		Ca ²⁺	none	none	none	none	none
Treat-	Grams per Liter	Sr ²⁺	none	none	none	3.0	0.9
ment	of:	WO ₄ -2	none	none	0.3	none	none
Compo-		NO ₃ -	8.9	7.6	9.0	8.0	7.3
sition		F-	0.1	none	0.1	none	0.1
Constit-		NO ₂ -	0.01	none	0.01	none	none
uents	•	NH ₄ OH	none	1.5	none	3.0	3.5
and		Temperature, °C	40	45	50	39	20
Process	Treatme	nt Time, Seconds	120	120	120	120	120
Condi-					l i		- 1
tions:							

Table 14: COMPARATIVE EXAMPLES 26 TO 30

			Comparative Example Number: 26 27 28 29 30								
			26	27	28	29	30				
	PREP.	ALENE®-ZN, g/l	1	none	none	none	none				
		Abbreviation	none	Zn2FeP2	Zn3P2	Zn2CaP2	Zn2FeP2				
	Phosphate	Particle size, µm	none	1.7	6.5	1.6	0.3				
	Particles:	Concentration, g/l	none	7	1	5	0.00001				
Surface	Water Soluble VA Polymer	Substance Name	polyvinyl alcohol	none	sulfonic acid- modified PVAlc	Copoly- mer with VA	Copoly- mer with VA				
Condi- tioning Treat-	or Derivative :	Comonomer with VA	none	none	none	maleic acid	crotonic acid				
ment Com-	•	Comonomer % by Weight	none	none	none	80	70				
position		Concentration, ppm	1	none	2,000	3,000	10				
Constit-	Salt con- stituent(s):	Chemical Formula	none	Na ₂ O•SiO 2 •5H ₂ O	none	Na ₂ CO ₃	Na ₃ PO ₄ •12H ₂ O				
Process		Concentration, g/l	none	1	none	5	10				
Condi-	Surfactant	Abbreviation	none	none	none	none	EO11NPE				
tions:	Constit- uents:	Concentration, g/l	none	none	none	none	2.0				
		ıt Temperature, °C	20	20	20	20	40				
	Treatm	ent Time, Seconds	30	30	30	30	120				
		PO ₄ 3-	10	15	20	18	16				
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4				
l		Mg ²⁺ Co ²⁺	2.0	none	none	none	2.5				
Phos-		Co ²⁺	none	1.0	none	none	none				
phate Conver-		Mn ²⁺	0.5	none	1.0	none	none				
sion		Ca ²⁺	none	none	none	1.5	none				
Treat-	Grams	Sr ²⁺	none	none	none	none	0.9				
ment	per Liter	WO ₄ -2	none	none	0.3	none	none				
Compo-	of:	NO ₃ -	8.3	7.6	9.0	8.0	7.3				
sition		F-	0.1	none	0.1	none	0.1				
Constit-	į	NO ₂ -	0.01	none	0.01	none	0.01				
uents		NH ₄ OH	none	1.5	none	3.0	none				
and		nt Temperature, °C	40	45	50	39	43				
Process Condi- tions:	Treatme	ent Time, Seconds	120	120	120	120	120				

Table 15: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR EXAMPLES 16 THROUGH 20

TEST OR OTHER RATING	SUBSTRATE		EXAM	APLE NUM	1BER	
	TESTED	16	17	18	19	20
Coating Appearance	CRS	+	+	+	+	+
	EG	+	+	+	+	+
	GA	+	+	+	+	+
Secondary (Water-Resistant)	CRS	++	++	++	++	++
Adherence	EG	++	++	+	++	++
	GA	++	++	+	++	++
	CRS	++	++	++	++	+
Resistance to Hot Salt Water	EG	++	++	++	++	++
	GA	++	++	++	++	++
	CRS	+	++	++	+	+
Resistance to Salt Spray	EG	++	+	++	+	++
	GA	++	+	++	+	++

Table 16: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR COMPARISON EXAMPLES 21 THROUGH 30

TEST OR OTHER RATING	SUB-	ATE TTE D 21 22 23 24 25 26 27 28 28 29 29 29 29 29 29 29 29 29 29 29 29 29									
	STRATE TESTE D	21	22	23	24	25	26	27	28	29	30
	CRS	×	+	×	×	×	+	×	×	×	×
Coating Appearance	_EG_	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	+	+	++	++	++	+	++	++	++	+
Secondary (Water-Resistant)	EG	×	×	×	×	×	×	×	×	×	×
Adherence	GA	×	×	×	×	×	×	×	×	×	×
	CRS	×	++	×	×	×	++	×	×	×	×
Resistance to Hot Salt Water	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	×	×	×	×	×	×	×	×	×	×
Resistance to Salt Spray	EG	×	+	×	×	×	+	×	×	×	×
	GA	×	×	×	×	×	×	×	×	×	×

Table 17: EXAMPLES 21 TO 25 with Type (4) Polymer Adhesion Promoting Agents

				I	Example N	umber:	
			21	22	23	24	25
	PREPA	LENE®-ZN, g/l	none	none	none	none	none
		Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
	Phosphate		0.5	0.5	1.7	0.6	0.5
	Particles	Concentration, g/l		1	1	5	10
	Monomer	R ^I	H	none	none	CH ₃	none
	with	R ²	C2H4OH	none	none	C3H7OH	none
Surface		Wt% in Polymer	100	none	none	20	none
Condi- tioning	Other Un- saturated	Monomer Name	none	maleic acid	acrylic acid	maleic acid	methacrylic acid
Treat-	Acid Monomer	Wt% in Polymer	none	80	100	80	50
Com-	Other Co- monomer	Monomer Name	none	vinyl acetate	none	none	styrene- sulfonic acid
position		Wt% in Polymer	none	20	none	none	50
Constit-	Polymer C	oncentration, ppm	1	500	2,000	1,500	5
uents and Process	Salt con- stituent(s)	Chemical Formula	MgSO ₄ •7H ₂ O	Na ₂ O • Si O ₂ • 5H ₂ O	none	КОН	Na ₃ PO ₄ •12H ₂ O
Condi-		Concentration, g/l	0.5	1	none	5	10
tions:	Surfactant		none	none	none	none	EOLINPE
tions.	Constit- uents	Concentration, g/l		none	none	none	2.0
1	Treatment	Temperature, °C	20	20	20	20	40
i	Treatme	nt Time, Seconds	30	30	30	30	120
		PO43-	10	15	20	18	16
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4
		Mg2+	2.0	none	none	none	2.5
Phos-		Mg2+ Co2+	none	1.0	none	none	none
phate		Mn ²⁺	0.5	none	1.0	none	none
Conver-		Ca ²⁺	none	none	none	1.5	none
sion	Grams	Sr ²⁺	none	none	none	none	0.9
Treat-	per Liter	WO₄-2	none	none	0.3	none	none
ment	of:	NO ₃ -	8.3	7.6	9.0	8.0	7.3
Compo-			0.1	none	0.1	none	0.1
sition		NO ₂ -	0.01	none	0.01	none	0.01
Constit-		NH ₄ OH	none	1.5	none	3.0	none
uents		Temperature, °C	40	45	50	39	43
and	Treatme	nt Time, Seconds	120	120	120	120	120
Process							
Condi-							
tions:						l	

Table 18: COMPARATIVE EXAMPLES 31 TO 35

				Compa	rative Exam	ple Number:	
			31	32	33	34	35
	PREPA	LENE®-ZN, g/I	none	none	none	none	none
	D	Abbreviation	Zn2FeP2	Zn3P2	Zn3P2	Zn2CaP2	Zn2FeP2
Į.	Phosphate	Particle size, µm	0.5	0.5	1.7	0.6	0.5
	Particles	Concentration, g/l R1	-5	I	1	5	10
1	Monomer	Ri	H	none	none	CH ₃	none
Surface	with,	R ²	C_2H_4OH		none	C3H7OH	none
Condi-	Formula (I)	Wt% in Polymer	100	none	none	20	none
tioning	Other Un- saturated	Monomer Name	none	maleic acid	acrylic acid	maleic acid	methacrylic acid
Treat-	Acid Monomer	Wt% in Polymer	none	80	100	80	50
ment Com-	Other Co- monomer	Monomer Name	none	vinyl acetate	none	none	styrenesul- fonic acid
position		Wt% in Polymer	none	20	none	none	50
Constit-	Polymer Co	oncentration, ppm		500	2,000	1.500	5
uents and	Salt con- stituent(s)	Chemical Formula	MgSO₄ •7H2O	Na ₂ O•Si O ₂ •5H ₂ O	none	Na ₂ CO ₃	Na3PO ₄ •12H ₂ O
Process		Concentration,	0.5	1	none	5	10
Condi-	Surfactant	Abbreviation	none	none	none	none	EOTINPE
tions:	Constit- uents	Concentration,	none	none	none	none	2.0
	Treatment	Temperature, C	20	20	20	20	40
	Treatmen	t Time, Seconds	30	30	30	30	120
		P(143-	11	15	1.0	18	16
		Zn ²⁺	0.1	7.0	2.0	1.5	1.4
		Zn2+ Mg2+	2.0	none	none	none	2.5
Phos-		Co2+ Mn2+	none	none	none	none	none
phate		Mn ²⁺	0.6	none	1.0	1.0	none
		Ca2+	none	none	none	none	none
Conver-		Sr2+	none	none	none	3.0	0.9
sion		₩O ₄ -2	none	none	0.3	none	none
Treat-		NO3-	8.9	7.6	9.0	8.0	7.3
ment	Grams	F	0.1	none	0.1	none	0.1
	per Liter	NO2-	0.01	none	0.01	none	none
Compo-	of:	NH4OH	none	1.5	none	3.0	3.5
sition	Treatment	Temperature, 'C	40	45	50	39	20
Constit-	Treatmen	t Time, Seconds	120	120	120	120	120
uents and Process Condi- tions:					.20	.20	120

Table 19: COMPARATIVE EXAMPLES 36 TO 40

				Comparativ	e Example	Number:	
			36	37	38	39	40
	PREP	ALENE®-ZN, g/I	T	none	none	none	none
		Abbreviation	none	Zn2CaP2	Zn3P2	Zn2CaP2	Zn2FeP2
Surface	Phosphate	Particle size, µm	none	0.8	6.8	0.6	0.5
Condi-	Particles	Concentration, g/l	none	10	I	5	0.0001
	Monomer	R!	H	none	none	CH3	none
tioning	with.	$\hat{\mathbf{R}}^2$	C ₂ H ₄ OH	none	none	C3H7OH	
Treat- ment	Formula (I)	Wt% in Polymer	100	none	none	20	none
Com-	Other Un- saturated	Monomer Name	none	none	acrylic acid	maleic acid	metha- crylic acid
position	Acid Monomer	Wt% in Polymer	none	none	100	80	50
Constit-	Other Co- monomer	Monomer Name	none	none	none	none	styrenesul -fonic acid
and		Wt% in Polymer	none	none	none	none	50
	Polymer	Concentration, ppm		none	2,000	3,000	5
Process Condi-	Salt con- stituent(s)	Chemical Formula	MgŜO₄ ●7H2O	Na ₂ O • SiO • 5 H ₂ O	none	Na ₂ CO ₃	Na3PO4 • 12H2O
tions:	bareacare(b)	Concentration, g/l	0.5	•3H2U			
	Surfactant	Abbreviation		1	none	5	10
	Constit-	Concentration, g/I	none	none	none	none	EOLINPE
	uents	Concentration, g/i	none	none	none	none	2.0
	Treatme	nt Temperature, °C	20	20	20	20	40
	Treatm	ent Time, Seconds	30	30	3ŏ	<u>3ŏ</u>	120
		PO/3-	ĬŎ	15	20	18	16
		Zn ²⁺	0.8	1.3	2.2	1.5	1.4
Phos-		Zn ²⁺ Mg ²⁺ Co ²⁺	2.0	none	none	none	2.5
phate		Co2+	none	1.0	none	none	none
		Mn2+	0.5	none	1.0	none	none
Conver-	Grams	Ca ²⁺	none	none	none	1.5	none
sion	per Liter	Sr ²⁺	none	none	none	none	0.9
Treat-	of:	WO ₄ -2	none	none	0.3	none	none
ment		NO3-	8.3	7.6	9.0	8.0	7.3
		F.	0.1	none	0.1	none	0.1
Compo-		NO ₂ -	0.01	none	0.01	none	0.01
sition		NH4ÖH	none	1.5	none	3.0	none
Constit-							
uents	Treatmen	it Temperature, °C	40	45	50	39	43
and	Treatm	ent Time, Seconds	120	120	120	120	120
Process				I	l		
					l		
Condi-							
tions:					l		1
					·		

Table 20: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR EXAMPLES 21 THROUGH 25

TEST OR OTHER RATING	SUBSTRATE		EXA	APLE NUM	1BER	
	TESTED	21	22	23	24	25
Coating Appearance	CRS	+	+	+	+	+
J	EG	+	+	+	+	+
	GA	+	+	+	+	+
Secondary (Water-Resistant)	CRS	++	++	++	++	++
Adherence	EG	++	++	+	++	++
	GA	++	++	+	++	++
	CRS	++	++	++	++	+
Resistance to Hot Salt Water	EG	++	++	++	++	++
	GA	++	++	++	++	++
	CRS	+	++	++	+	+
Resistance to Salt Spray	EG	++	+	++	+	++
	GA	++	+	++	+	++

Table 21: APPEARANCE OF THE CONVERSION COATING AND RESULTS OF PAINTING PERFORMANCE TESTING FOR COMPARISON EXAMPLES 31 THROUGH 40

TEST OR OTHER RATING	SUB-		C	OMPAR	ISON	EXAN	1PLE	NUM	BER		
	STRATE TESTE D	31	32	33	34	35	36	37	38	39	40
	CRS	×	+	×	×	×	+	×	×	×	×
Coating Appearance	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	++	+	++	++	++	+	++	++	++	+
Secondary (Water-Resistant)	EG	×	×	×	×	×	×	×	×	×	×
Adherence	GA	×	×	×	×	×	×	×	×	×	×
	CRS	×	++	×	×	×	++	×	×	×	×
Resistance to Hot Salt Water	EG	×	+	×	×	×	+	×	×	×	+
	GA	×	+	×	×	×	+	×	×	×	+
	CRS	×	×	×	×	×	×	×	×	×	×
Resistance to Salt Spray	EG	×	+	×	×	×	+	×	×	×	×
	GA	×	×	×	×	×	×	×	×	×	×

CLAIMS

- 1. A process for forming a phosphate conversion coating on a metal substrate surface, said process comprising the following operations:
- (I) contacting the metal substrate surface with an aqueous liquid surface conditioning composition that comprises, preferably consists essentially of, or more preferably consists of, water and the following components:
- (I.A) dispersed solid phosphate particles that:
 - (i) have a diameter no greater than 5 μm; and
 - comprise at least one substance selected from the group consisting of phosphates that contain at least one type of divalent or trivalent metal cations:

and

- (I.B) as adhesion-promoting component, at least one selection from the group consisting of the following subgroups:
 - (1) monosaccharides, polysaccharides, and derivatives thereof;
 - phosphorus containing solutes selected from the group consisting of orthophosphoric acid, condensed phosphoric acids, and organophosphonic acid compounds;
 - (3) water-soluble polymers that are homopolymers or copolymers of vinyl acetate and derivatives of these homopolymers and copolymers; and
 - (4) copolymers and polymers afforded by the polymerization of:
 - (a) at least one selection from:
 - -- monomers, exclusive of vinyl acetate, that conform to general chemical formula (I):

$$H_2C=C-COOR^2$$
 (I),

where R^1 = H or CH_3 and R^2 = H, C_1 to C_5 alkyl, or C_1 to C_5 hydroxyalkyl, and

- other α,β-unsaturated carboxylic acid monomers; and, optionally,
- (b) not more than 50 % by weight of monomers that are not vinyl acetate and are not within the description of part (a) immediately above but are copolymerizable with said monomers that are

within the description of said part (a);

and

- (II) contacting the metal substrate surface as conditioned in operation (I) as described above with a nickel-free phosphate conversion treatment bath that comprises water and the following amounts of the following components:
- (II.A) from 0.5 to 5 g/l of zinc cations;
- (II.B) from 5 to 30 g/l of phosphate ions; and
- (II.C) a component of conversion accelerator.
- 2. A process according to claim 1, wherein the phosphate conversion treatment bath also contains from 0.1 to 3.0 g/l of at least one type of ions selected from the group consisting of magnesium ions, cobalt ions, manganese ions, calcium ions, tungstate ions, and strontium ions.
- 3. A process according to claim 2, wherein the concentration of component (I.A) is from 0.001 to 30 g/l and the concentration of component (I.B) is from 1 to 2,000 ppm.
- A process according to claim 1, wherein the concentration of component (I.A) is from 0.001 to 30 g/l and the concentration of component (I.B) is from 1 to 2.000 ppm.

ABSTRACT OF THE DISCLOSURE

A metal surface on which a phosphate conversion coating is to be formed and which has been surface conditioned by contact with a liquid surface conditioner composition that contains dispersed fine particles of solid phosphate of at least one divalent or trivalent cations type and an adhesion promoting agent. After such conditioning, a very high quality conversion coating can be formed on the surface by contact with a nickel-free liquid phosphating composition that contains at least acid, zinc cations, and phosphate anions and optionally and preferably also contains other materials.

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DECLAR/	ATION FOR	First Named Inventor	HirokatsuB.	ANNAI		
		COM	PLETE IF KNOW			
UTILITY	OR DESIGN	Application Number				
PATENT AF	PLICATION	Filing Date				
y Declaration	OR Declaration	Group Art Unit	 			
Submitted with Initial Filing	Submitted after Initial Filing	Examiner Name				
I believe I am the original, first and the subject matter which is da PROCESS FOR FO the specification of which is attached hereto OR X was filed on (MM/DD/Y/Application No. PCT I hereby state that I have review amendment specifically referre I acknowledge the duty for discharge I have been provided in the subject of th	YY) 08/16/2000 /US00/22335 and wed and understand the contents of	insted below) or an original, first and on the invention entitled CONVERSION COATIN the Invention) as United Si was amended on the above identified specification, patentability as defined in Title 37- code §119(a)-(d) or §395(b) of any	NG ON META	umber or PCT International (if , as amended by any equilations, § 1 56 s) for patent or inventor's		
and have also identified below, b having a filing date before that of	y checking the box, any foreign appl the application on which priority is o	ication for patent or inventor's certical	ficate, or of any PC	T International application		
Prior Foreign Application Number(s)	Country	Foreign Filing Date (MM/DD/YYYY	Priority Not Claimed	Certified Copy Attached? YES NO		
H11-230060	Japan	08/16/1999		X		
	in numbers are listed on a suppleme					
	itle 35, United States Code §119(e)	of any United States provisional a				
Application Number(s)	Filing Date (MW/DD/YYYY)		Additional provision application number are listed on a supplemental prior sheet attached he	ers		

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DECLARATION

Page 2

I hereby claim the benefit under Title 35, United States Code §120 of any United States application(s), or §365(c) of any PCT international application

designating the United States of Americ prior United States or PCT international duty to disclose information which is may the filling date of the prior application an	application in the miterial to patentability	anner prov as defined	ided by t in Title	the first paragra 37, Code of Fe	ph of Title 35, deral Regulate	United Stat	es Code §11	2 1 acknowle	dge the					
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Additional U.S. or PCT international application numbers are listed on a supplemental priority sheet attached hereto														
As a named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith														
Firm Name RUSHGEP or Natural OR														
X List Attomey(s) and/or agent(s) name and registration number below														
Name		Registra Numb			-	Name		Registrati Numb						
Stephen D. Harper Kimberly R. Hild		33,24 39,22		Glenn E.		33,539	<u></u>							
Additional attorney(s) and/or age	ent(s) named on a su	pplementa	l sheet a	ittached hereto										
Please direct all correspondence to Customer or label OR														
Name Stephen D. Ha														
Address <u>Henkel Corpor</u>														
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City Gulph Mills				State	PA_	·		=	19406					
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I hereby declare that all statements ma- true; and further that these statements imprisonment, or both, under Section 1 application or any patent issued thereor	were made with the I 001 of Title 18 of the	knowledge	that will	ul talse statem	ents and the like	ke so made	are punishab	ole by fine or						
Name of Sole or First Inver	tor:				A petitio	n has been	en tiled for this unsigned inventor							
Given Hirokatsu					BANNAI	_	Suffix e g. Jr							
Inventor's Signature	zu BA	NN	AI			Date	2.	5, 201)2					
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City Hiratsuka-shi	Pref	J	1	54-0012	Country	JP	Applicant Authority							
Additional inventors are be	eing named on s	suppleme	ental s	heet(s) atta	ched heret	0								

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4	DECLARATION ADDITIONAL INVENTOR(S) Supplemental Sheet																		
i	Namo	Name of Additional Joint Inventor, if any:																	
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	Name			ко				nitial Name NAGASHIN						e.g. Jr.					
\(\)	Inventor's Signature Yasuhiba (M	aga	st	rim	a		Date 2.5.200						
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